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## 40 C.F.R. § 60.106

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### Test methods and procedures.

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(a) In conducting the performance tests required in § 60.8, the owner or operator shall use as reference methods and procedures the test methods in appendix A of this part or other methods and procedures as specified in this section, except as provided in § 60.8(b).

(b) The owner or operator shall determine compliance with the particulate matter (PM) standards in § 60.102(a) as follows:

(1) The emission rate (E) of PM shall be computed for each run using the following equation:

$$E = \frac{c_s Q_{sd}}{KR_c}$$

Where:

E = Emission rate of PM, kg/Mg (lb/ton) of coke burn-off.  $c_s$  = Concentration of PM, g/dscm (gr/dscf).  $Q_{sd}$  = Volumetric flow rate of effluent gas, dscm/hr (dscf/hr).  $R_c$  = Coke burn-off rate, Mg/hr (ton/hr) coke. K = Conversion factor, 1,000 g/kg (7,000 gr/lb).

(2) Method 5B or 5F is to be used to determine particulate matter emissions and associated moisture content from affected facilities without wet FGD systems; only Method 5B is to be used after wet FGD systems. The sampling time for each run shall be at least 60 minutes and the sampling rate shall be at least 0.015 dscm/min (0.53 dscf/min), except that shorter sampling times may be approved by the Administrator when process variables or other factors preclude sampling for at least 60 minutes.

(3) The coke burn-off rate ( $R_c$ ) shall be computed for each run using the following equation:

$$R_c = K_1 Q_r (\%CO_2 + \%CO) + K_2 Q_a - K_3 Q_r (\%CO/2 + \%CO_2 + \%O_2) + K_3 Q_{oxy} (\%O_{oxy})$$

Where:

$R_c$  = Coke burn-off rate, kilograms per hour (kg/hr) (lb/hr).  $Q_r$  = Volumetric flow rate of exhaust gas from fluid catalytic cracking unit regenerator before entering the emission control system, dscm/min (dscf/min).  $Q_a$  = Volumetric flow rate of air to fluid catalytic cracking unit regenerator, as determined from the fluid catalytic cracking unit control room instrumentation, dscm/min (dscf/min).  $Q_{oxy}$  = Volumetric flow rate of  $O_2$  enriched air to fluid catalytic cracking unit regenerator, as determined from the fluid catalytic cracking unit control room instrumentation, dscm/min (dscf/min).  $\%CO_2$  = Carbon dioxide concentration in fluid catalytic cracking unit regenerator exhaust, percent by volume (dry basis).  $\%CO$  = CO concentration in FCCU regenerator exhaust, percent by volume (dry basis).  $\%O_2$  =  $O_2$  concentration in fluid catalytic cracking unit regenerator exhaust, percent by volume (dry basis).  $\%O_{oxy}$  =  $O_2$  concentration in  $O_2$  enriched air stream inlet to the fluid catalytic

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cracking unit regenerator, percent by volume (dry basis).  $K_1$  = Material balance and conversion factor, 0.2982 (kg-min)/(hr-dscm-%) [0.0186 (lb-min)/(hr-dscf-%)].  $K_2$  = Material balance and conversion factor, 2.088 (kg-min)/(hr-dscm) [0.1303 (lb-min)/(hr-dscf)].  $K_3$  = Material balance and conversion factor, 0.0994 (kg-min)/(hr-dscm-%) [0.00624 (lb-min)/(hr-dscf-%)].

(i) Method 2 shall be used to determine the volumetric flow rate ( $Q_T$ ).

(ii) The emission correction factor, integrated sampling and analysis procedure of Method 3B shall be used to determine  $CO_2$ , CO, and  $O_2$  concentrations.

(4) Method 9 and the procedures of § 60.11 shall be used to determine opacity.

(c) If auxiliary liquid or solid fossil-fuels are burned in an incinerator-waste heat boiler, the owner or operator shall determine the emission rate of PM permitted in § 60.102(b) as follows:

(1) The allowable emission rate ( $E_S$ ) of PM shall be computed for each run using the following equation:

$$E_S = F + A (H/R_C)$$

Where:

$E_S$  = Emission rate of PM allowed, kg/Mg (lb/ton) of coke burn-off in catalyst regenerator.  $F$  = Emission standard, 1.0 kg/Mg (2.0 lb/ton) of coke burn-off in catalyst regenerator.  $A$  = Allowable incremental rate of PM emissions, 43 g/GJ (0.10 lb/million Btu).  $H$  = Heat input rate from solid or liquid fossil fuel, GJ/hr (million Btu/hr).  $R_C$  = Coke burn-off rate, Mg coke/hr (ton coke/hr).

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